Pollution of water by toxic substances is one of the major reasons concerning human health as well as the environmental quality. In terms of pollution, mining activities represent a serious threat. Countries of the middle Europe, where extraction of mineral resources takes place for a long period, have to solve the problems of wastewater containing whole spectra of heavy metals, which are dangerous to the environment. Finding of the new and cheap ways of wastewater contaminated by heavy metals treatment can increase the quality of the environment in the affected localities and thus prevent adverse effects on fauna, flora or human beings. Sorption techniques belong to a cost effective methods that are able to effectively remove heavy metals. For the overall understanding of the sorption process, it is necessary to characterize and determine the properties of the used adsorbents. The paper deals with characterization of natural zeolite before and after sorption process under acidic conditions. The zeolite was characterized using Fourier transform infrared spectroscopy, X-ray diffraction, scanning electron microscopy and N₂ adsorption/desorption isotherms.

**Keywords:** zeolite, sorption, XRF, XRD, SEM, specific surface area

### 1. Introduction

The development of human society after 18\(^{th}\) century is associated with metals. Technology of extraction and processing of heavy metals is essential for...
many areas of industry. Naturally, the extraction, processing and cleaning of impurities give the metals not only a new form, but also cause their intensive distribution in the environment, which represents a huge threat.

Ion-exchange sorption is one of the basic process technologies of liquid waste, in which the fixing of metal cations in the suitable form for deposition in the storage site is ensured [1]. Finding of cheap and efficient materials from natural resources is therefore necessary.

Natural zeolites are hydrated aluminosilicate minerals of a porous structure with valuable physicochemical properties, such as cation exchange, molecular sieving, catalysis and sorption [2]. The sorption properties of the zeolites had been known for the decades. After the large-scale application of x-ray powder diffraction in the second half of 20th century a huge reserves of zeolites began to appear and subsequently have been studied and utilized as adsorbents for the removal of heavy metals in many countries [3], [4] and [5].

The aim of this study was to investigate possibilities of application of Slovak natural zeolite for removal of heavy metal ions from aqueous solutions. In specific, Cu(II) was selected as a model ion due to common presence of this cation in the acid mine drainage. Zeolite was also characterized using different methods in order to determine the changes caused by adsorption/ion-exchange process.

2. Materials and methods

2.1. Zeolite samples preparation

In this study a natural non-modified zeolite from locality of Nizny Hrabovec (Slovakia) was used. The different fractions were prepared by milling of commercial product with granularity of 2.5 to 5 mm (Zeocem, a.s.; Bystre, Slovakia) by planetary mill (Desk – top planetary ball Miller SFM-1) at 290 rpm (tray rotating) and 580 rpm (grinding jars rotating) for 18 min. After that sieve analysis for the purpose of separation of different fractions was performed. Sieves were shaken in a mechanical shaker for 10 minutes to provide complete separation. The separated fraction of zeolite was washed in deionized water in order to eliminate eventually present dust. Samples were dried at 105 °C for 17 h and then allowed to cool in the desiccators before their using in experiments.

2.2. Apparatus and instrumentation

- A Colorimeter DR890 (HACH LANGE, Germany) with appropriate reagent was used to determine amount of dissolved Cu(II).
- The basic chemical composition of zeolite was investigated by X-ray fluorescence analysis (XRF) using SPECTRO iQ II (Ametek, Germany) with SDD silicon drift detector with resolution of 145 eV at 10 000 pulses.
• IR spectra were measured by Alpha FT-IR Spectrometer with ALPHA’s Platinum ATR single reflection diamond ATR module (Bruker, Germany).
• Mineralogical analysis of the natural zeolite samples was carried out by X-Ray Diffraction (XRD) using diffractometer Bruker D2 Phaser (Bruker AXS, GmbH, Germany) in Bragg-Brentano geometry (configuration Theta-2Theta), using the 1.54060 Å CuKα radiation, Ni Kβ filters and scintillation detector at a voltage of 30 kV and 10 mA current. Scan conditions: recording time about 4.5 hours, a step size of 0.02° (2Θ) and step time of 5 s. The XRD patterns were processed using the software Diffrac.EVA v. 2.1. The ICDD PDF database (ICDD PDF – 2 Release 2009) was utilized for the phase identification.
• SEM (Tescan – VEGA3 LMU) with EDX analysis (Bruker, Germany) was used for determination of composition and structure of the zeolite surface.
• Specific surface area was estimated by low temperature gas adsorption using nitrogen gas (Quantachrome NOVA 1000e, USA).

2.3. Adsorbate solution preparation

Synthetic solutions of Cu(II) were prepared from CuSO₄·5H₂O (A.R.). Working solutions were prepared by further dilution to the desired initial concentration (50 mg/L). The initial pH of each solution was adjusted to the required value (pH ≈ 4) by adding 0.001M H₂SO₄. It should be noted that sulphate anions are not forming precipitates or complexes with copper cations at the test conditions and are considered to be inert.

2.4. Batch adsorption experiment

For the purpose of removal efficiency investigation and also preparation of zeolite sample with adsorbed cations, batch adsorption experiment was carried out. Zeolite (fraction below 0.063 mm) was mixed with single-component solutions containing 50 mg/L of Cu(II). Batch experiments were carried out at room temperature (23±0.2°C) in beakers, batch rate: 1 g of zeolite per 100 mL of solution. After 24 hours reaction time, sorbents were removed by filtration through a laboratory filter paper for qualitative analysis and residual concentration of copper was determined by colorimetric method. Used zeolite was separated and dried at 105 °C for 17 h and then allowed to cool in the desiccators before their further characterization.

2.5. Fixed – bed adsorption experiment

Fixed – bed column used in this study was made of Pyrex glass tube with the inner and outer diameters of 4.0 and 4.5 cm, respectively ended by coarse porosity fritted glass disc. A known quantity (50 g) of the zeolite (1 – 2 mm and 2 – 4 mm, respectively) was packed in the column to yield a bed height of 4 cm.
Solution containing copper of 50 mg/L flowed by gravity downward through the column at a filtration velocities of 0.3 and 1.3 mL/sec (for 1 – 2 mm and 2 – 4 mm fraction, respectively), controlled by a couple of valves. The effluents at the outlet of the column were collected at regular time intervals and the Cu(II) concentrations were measured using colorimetric method. All experiments were performed at room temperature (23±0.2°C).

3. Results

3.1. Characterization of natural zeolite

In order to determine the basic characteristics of natural zeolite and changes after the sorption process several measurements were carried out. The results from X-ray fluorescence (XRF) analysis, X-Ray Diffraction (XRD), Infrared spectroscopy (FTIR), scanning electron microscopy (SEM) and specific surface area (SSA) measurements are presented.

3.1.1. XRF

XRF analysis was used to determine of chemical composition of zaolite samples. The chemical composition of the zeolite declared by the manufacturer (Zeocem, a.s.) and results from X-ray fluorescence analysis are listed in Table 1.

Table 1. Chemical composition of zeolite (declared data by manufacturer and results of XRF analysis)

<table>
<thead>
<tr>
<th>Constituent</th>
<th>SiO₂</th>
<th>Al₂O₃</th>
<th>CaO</th>
<th>K₂O</th>
<th>Fe₂O₃</th>
<th>MgO</th>
<th>Na₂O</th>
<th>TiO₂</th>
</tr>
</thead>
<tbody>
<tr>
<td>Declared content (mass %)</td>
<td>65.00 – 73.00</td>
<td>11.50 – 13.10</td>
<td>2.70 – 5.20</td>
<td>2.20 – 3.40</td>
<td>0.70 – 1.90</td>
<td>0.60 – 1.20</td>
<td>0.20 – 1.30</td>
<td>0.10 – 0.30</td>
</tr>
<tr>
<td>XRF analysis (mass %)</td>
<td>64.10</td>
<td>9.89</td>
<td>2.99</td>
<td>2.71</td>
<td>1.34</td>
<td>0.73</td>
<td>-</td>
<td>0.15</td>
</tr>
</tbody>
</table>

3.1.2. XRD

Mineralogical analysis of the natural zeolite samples (before and after sorption) was carried out using X-Ray Diffraction. The results showed that the natural zeolite contained clinoptilolite in the majority, and small quantities of silicon oxides (cristobalite and quartz), feldspar and illite (see Fig. 1). From the pattern is also evident that the sorption does not affect the mineralogical structure; patterns are identical.
3.1.3. FTIR

The characterization of zeolites by FTIR technique is based on the presence of bands in three regions. A higher one corresponds to the OH stretching modes (3650 – 3450 cm\(^{-1}\)) with an additional band at 1620 – 1640 cm\(^{-1}\) (Lewis sites).
This region is assigned H-O-H bending of the water molecules (zeolitic water) in channels of the samples [6]. The middle zone (1200 – 900 cm\(^{-1}\)) is characterized by strong bands attributed basically to the TO\(_4\) (T = Al, Si) stretching modes whereas the corresponding bending modes of the 3D covalent arrangement are observed below 700 cm\(^{-1}\) [7].

As it is seen in Fig. 2, there is no difference between IR spectrum of pure zeolite and after sorption of copper thus there are not changes in chemical structure and also the precipitate is not present.

### 3.1.4. SEM

Characterization of structure and morphology of zeolite was observed by SEM with EDX. Fig. 3 represents the morphology of particulate substances of zeolite (left: pure zeolite; right: zeolite after sorption). As is shown in this figure, the structure is almost identical in both samples.

![Fig. 3. Structure of zeolite (left: before sorption; right: after sorption)](image)

Rys. 3. Struktura zeolitu (z lewej: przed sorpcją; po prawej: po sorpcji)

The presence of Cu(II) on the surface of zeolite after the sorption has been proved by energy dispersive microanalysis (see results in Table 2.) According to ion – exchange background of the process, it can be observed a little decrease in concentration of exchangeable cations (K, Mg, Ca) after the sorption process.
Table 2. Chemical composition of zeolite by SEM/EDX

<table>
<thead>
<tr>
<th>Element</th>
<th>O</th>
<th>Si</th>
<th>K</th>
<th>Al</th>
<th>Mg</th>
<th>Fe</th>
<th>Ca</th>
<th>Cu</th>
</tr>
</thead>
<tbody>
<tr>
<td>Pure zeolite</td>
<td>38.8</td>
<td>38.2</td>
<td>5.2</td>
<td>7.7</td>
<td>0.3</td>
<td>5.2</td>
<td>4.6</td>
<td>-</td>
</tr>
<tr>
<td>Zeolite after sorption</td>
<td>38.1</td>
<td>40.0</td>
<td>4.7</td>
<td>7.9</td>
<td>0.2</td>
<td>4.4</td>
<td>3.2</td>
<td>1.07</td>
</tr>
</tbody>
</table>

3.1.5. Specific surface area

One of the many properties used to characterize adsorbents is the specific surface area (SSA). SSA plays an important role in adsorption processes; however, there are other mechanisms that can influence the progress of adsorption (e.g., ion-exchange abilities, complexation, chelation, etc.).

In order to evaluate the influence of grinding, estimation of SSA of different zeolite fractions by physisorption of nitrogen gas at 77 K according to the BET method was carried out. Degassing of zeolite was carried out with respect of their thermal stability determined by thermal analyzer (Netzsch STA 449 F3, Germany). The results are presented in Table 3.

Table 3. Specific surface areas of different zeolite fractions

<table>
<thead>
<tr>
<th>SSA (m²/g)</th>
<th>2 – 4 mm</th>
<th>1 – 2 mm</th>
<th>below 0.063 mm</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>24.97</td>
<td>27.61</td>
<td>28.35</td>
</tr>
</tbody>
</table>

As can be seen, the differences between fractions are minimal, in addition another measurement of the zeolite sample after the sorption process was also carried out. Despite after the 90% efficiency of copper removal, the change in specific surface area was not observed. This fact shows us an indication of the ion-exchange background of the process. From the shape of adsorption/desorption curves (Fig. 4) it can be said, that the zeolite exhibit microporous structure with the pore size predominantly under 1 nm.
3.2. Batch experiment

Batch adsorption experiment was performed in order to evaluate sorption efficiency of zeolite in static conditions. The percentage adsorption (%) was calculated using the following equation:

\[
\text{\% Adsorption} = \left( \frac{C_0 - C_e}{C_0} \right) \times 100 \%
\]

where, \( C_0 \) is the initial concentration of copper ions (mg/L) and \( C_e \), equilibrium concentration of copper ions (mg/L). Zeolite exhibit efficiency around 90 % after 24 h contact time with batch rate of 1g / 100 mL.

3.3. Fixed – bed column experiments

Adsorption of copper by zeolite is presented in the form of breakthrough curves (Figure 5). According to the results of previous experiments with 2 – 4 mm fraction, flow rate of 1.3 mL/sec is too high, since breakthrough occurs faster and with less sharpened boundaries. It was necessary to reduce the flow rate using the smaller fraction of zeolite which has proved as a successful approach (see Fig. 5).

Lower flow rate results in high residence times in the column. It is well known that, because of the relatively slow loading kinetics of zeolites, relatively
long residence times are needed [8]. In addition it is well known that decreasing in particle size improves the performance of adsorption and ion exchange [9]. This improvement is due to the extension of surface area (see Table 3) and better access to easily removable exchangeable cations in the zeolite structure.

4. Conclusions

Natural zeolites are important low cost and wide available materials for water and wastewater treatment. Due to the nature of cation exchange, zeolites exhibit high performance in adsorption of different cations in aqueous solution.

In this study, the natural zeolite (clinoptilolite) from Slovakia (Nizny Hrabovec) was characterized using different methods. A batch and fixed – bed systems were used to describe the adsorption properties. The efficiency of Cu(II) sorption was at satisfactory level (90 % for the batch system and 60 % after 80 batch volumes in the dynamic conditions), in addition the competitive adsorption in the process of ion - exchange between copper and hydrogen cations was observed.

Overall, from the results of this study imply that the adsorption under acidic condition does not affect the structure of zeolite. As a result of ion – exchange only one change in chemical composition using by SEM/EDX was observed.

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